

Asymptotic Model Reduction

Why Mathematicians Have An Important Role in Electrochemistry

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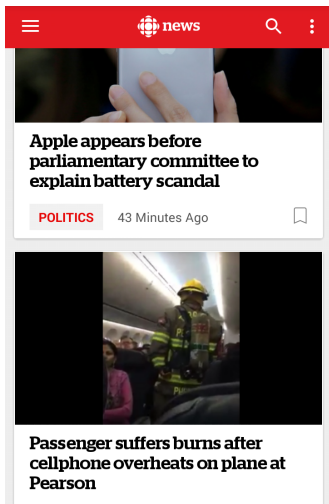
PIMS Workshop on Mathematical Sciences and Clean Energy
Applications



Acadamh Ríoga na hÉireann
Royal Irish Academy

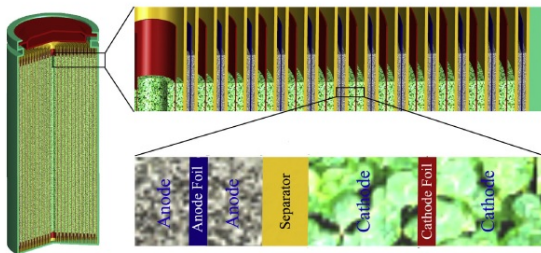
May 23, 2019

Introduction



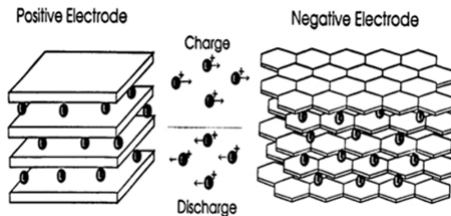
- Lithium-ion batteries power many of today's electronic devices
- Expected to play a key role in emerging technologies
- Advantages include long lifetime, high energy density, low self-discharge rates
- Unfortunately have been at the center of several controversies

What is an LiB?

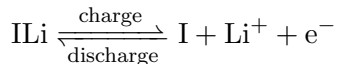


- A battery is composed of two electrodes and an electrolyte
- **P**ositive electrode (cathode on discharge)
- **S**eparator - non-conductive region filled with electrolyte
- **N**egative electrode (anode on discharge)

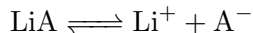
What is an LiB?



Electrodes:



Electrolyte:



Modelling Strategies

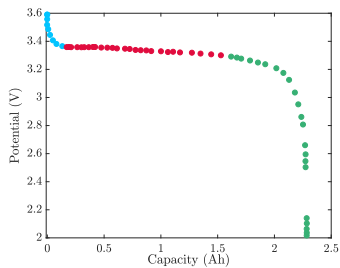
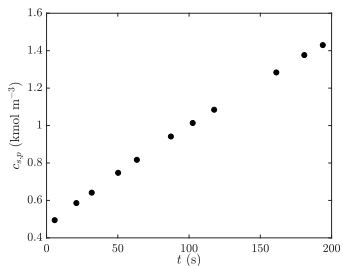
Two types of models are typically used:

- Equivalent circuit models (fast but not robust)
- Detailed electrochemical models (robust but not fast)

Can we use best of both worlds? Yes, asymptotic reduction!

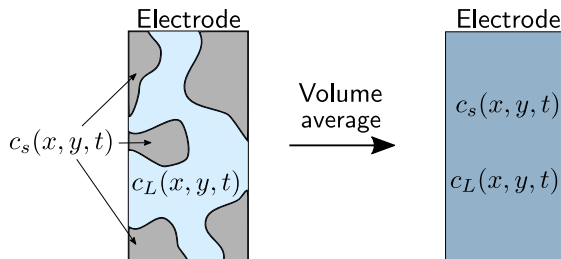
- Exploit small parameters to extract dominant terms and reduce equation complexity

Data



Model Approach

We use a volume averaging approach



Conserve mass, charge and factor in electrochemistry

What is an LIB?

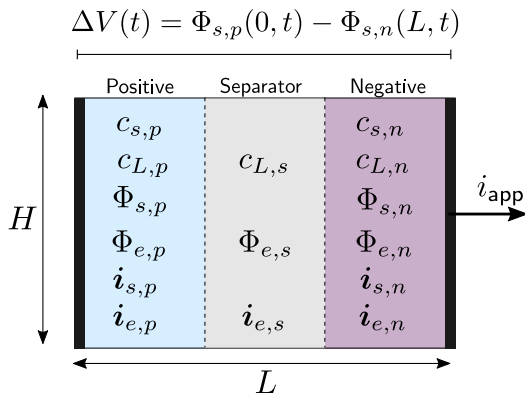


Figure: c concentration; Φ electric potential; i current density; i_{app} discharge current; ΔV voltage drop across cell

Model Equations

$$\frac{\partial}{\partial t}(\phi_{a,i}c_{a,i}) = \nabla \cdot (\phi_{a,i}D_{a,i}\nabla c_{a,i}) + \frac{1}{F}\nabla \cdot (\phi_{a,i}\mathbf{i}_{a,i}),$$

$$\mathbf{i}_{a,i} = -\sigma_{a,i}\nabla\Phi_{a,i},$$

$$\nabla \cdot (\phi_{a,i}\mathbf{i}_{a,i}) = -a_i \left(\bar{g}_i + C_{\Gamma,i} \frac{\partial}{\partial t}(\Phi_{a,i} - \Phi_{e,i}) \right),$$

$$\frac{\partial}{\partial t}(\phi_{e,i}c_{L,i}) = \nabla \cdot (\phi_{e,i}D_{L,i}\nabla c_{L,i} + \phi_{e,i}\mu_L F c_{L,i}\nabla\Phi_{e,i}) + \frac{1}{F}\nabla \cdot (\phi_{e,i}\mathbf{i}_{e,i}),$$

$$\mathbf{i}_{e,i} = F(\mathbf{N}_{L,i} - \mathbf{N}_{A,i}),$$

$$\nabla \cdot (\phi_{e,i}\mathbf{i}_{e,i}) = a_i \left(\bar{g}_i + C_{\Gamma,i} \frac{\partial}{\partial t}(\Phi_s - \Phi_e) \right),$$

$$\frac{\partial}{\partial t}(\phi_{e,s}c_{L,s}) = \nabla \cdot (\phi_{e,s}D_{L,s}\nabla c_{L,s} + \phi_{e,s}\mu_L F c_{L,s}\nabla\Phi_{e,s}),$$

$$\mathbf{i}_{e,s} = F(\mathbf{N}_{L,s} - \mathbf{N}_{A,s}),$$

$$\nabla \cdot (\phi_{e,s}\mathbf{i}_{e,s}) = 0.$$

Reaction Kinetics

Chemical reaction $r = k_{a,i}c_{a,i} - k_{L,i}c_{L,i} \left(\frac{c_{a,i}^{\max} - c_{a,i}}{c_{a,i}^{\max}} \right)$

Butler-Volmer:

$$\bar{g}_i = j_{0,i}(c_{a,i}, c_{L,i}) \left(\exp \left[\frac{(1 - \beta_i)F}{RT} \eta_i \right] - \exp \left[\frac{-\beta_i F}{RT} \eta_i \right] \right),$$

$$\eta_i = \Phi_{a,i} - \Phi_{e,i} - \frac{RT_a}{F} U_i,$$

- $j_{0,i}$ - exchange current density
- U_i - Open Circuit Potential

Reduction Approach

- Non-dimensionalise
- Several dimensionless numbers appear
 - $L/H \ll 1$: problem can be reduced to one dimension
 - $D_{s,i}/D_L \ll 1$: solid concentration spatially uniform
 - $(i_{\text{app}}LF)/(RT_a\sigma_i) \ll 1$: electric potentials spatially uniform
- Some small numbers are important
 - Capacitance \mathcal{C}_i
 - Concentration gradients $\gamma = \Delta c/c_{L0}$
- Liquid problem reaches an $\mathcal{O}(1)$ steady state in $\mathcal{O}(1)$ time

Composite Reduced Model

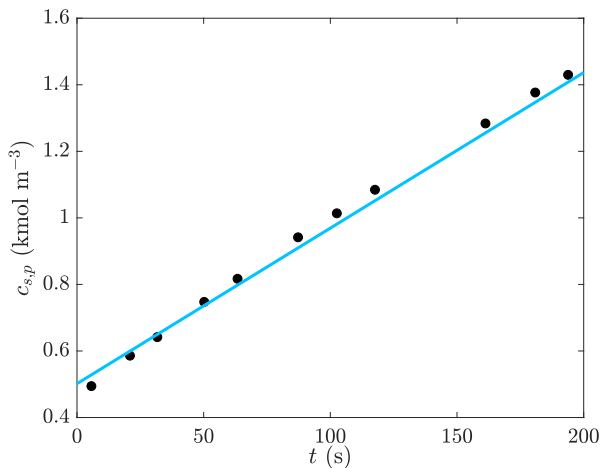
$$c_{a,n} = c_{a,n}^0 - \frac{\int_0^t i_{\text{app}}(\tau) d\tau}{F\phi_{a,n}(L - X_n)}, \quad c_{a,p} = c_{a,p}^0 + \frac{\int_0^t i_{\text{app}}(\tau) d\tau}{F\phi_{a,p}X_p}$$

Single ODE for potential in each electrode

$$C_n \frac{d\Phi_{a,n}}{dt} + \bar{g}_n(\Phi_{a,n}, c_{a,n}) = \frac{i_{\text{app}}}{a_n(L - X_n)}, \quad \Phi_{a,n}(0) = U_n(c_{a,n}^0/c_{a,n}^{\text{max}}),$$

$$C_p \frac{d\Phi_{a,p}}{dt} + \bar{g}_p(\Phi_{a,p}, c_{a,p}) = -\frac{i_{\text{app}}}{a_p X_p}, \quad \Phi_{a,p}(0) = U_p(c_{a,p}^0/c_{a,p}^{\text{max}})$$

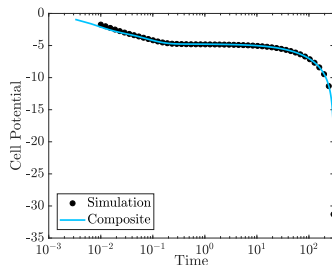
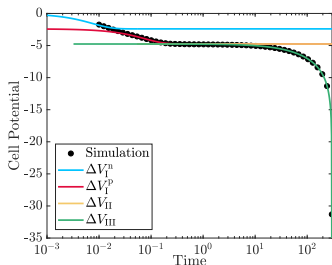
Electrode- "Data"



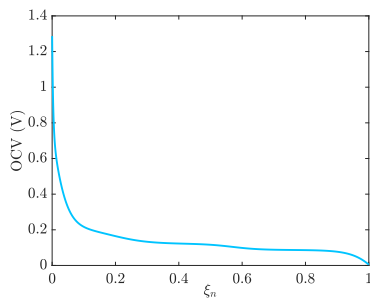
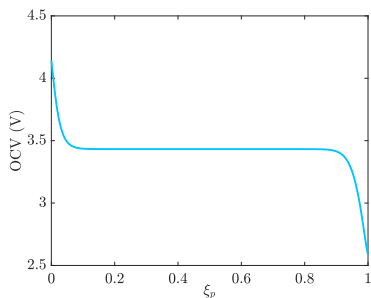
Summary of asymptotic regimes

Asymptotic analysis reveals three key regimes of battery operation:

- 1 $t \ll 1$: Formation of double charging layers due to instantaneous application of current to cell
- 2 $t = O(1)$: Onset of (de)lithiation of electrodes and diffusive transport through separator
- 3 $t \gg 1$: Electrode saturation and depletion



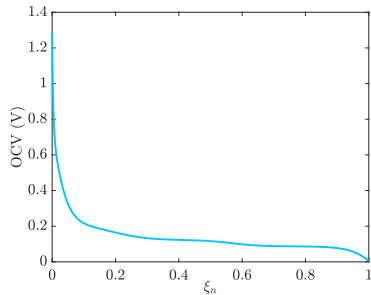
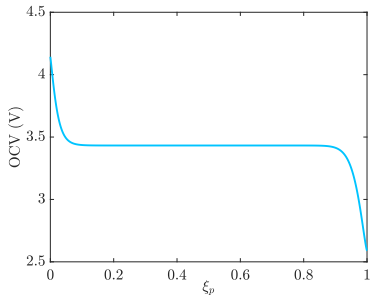
Open Circuit Potential



$$C_n \frac{d\Phi_{a,n}}{dt} + \bar{g}_n(\Phi_{a,n}, c_{a,n}) = \frac{i_{\text{app}}}{a_n(L - X_n)}, \quad \Phi_{a,n}(0) = U_n(c_{a,n}^0/c_{a,n}^{\text{max}}),$$

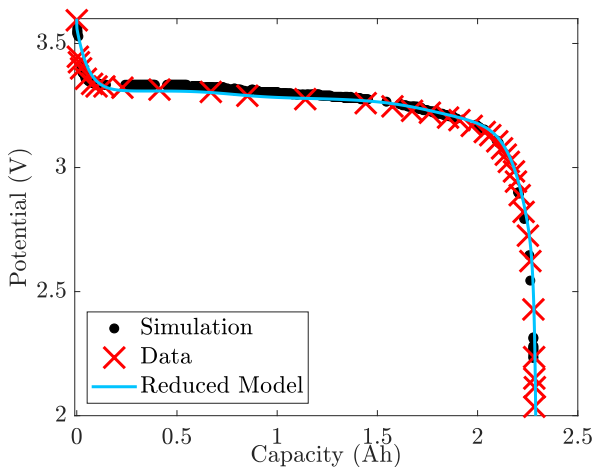
$$C_p \frac{d\Phi_{a,p}}{dt} + \bar{g}_p(\Phi_{a,p}, c_{a,p}) = -\frac{i_{\text{app}}}{a_p X_p}, \quad \Phi_{a,p}(0) = U_p(c_{a,p}^0/c_{a,p}^{\text{max}})$$

Open Circuit Potential

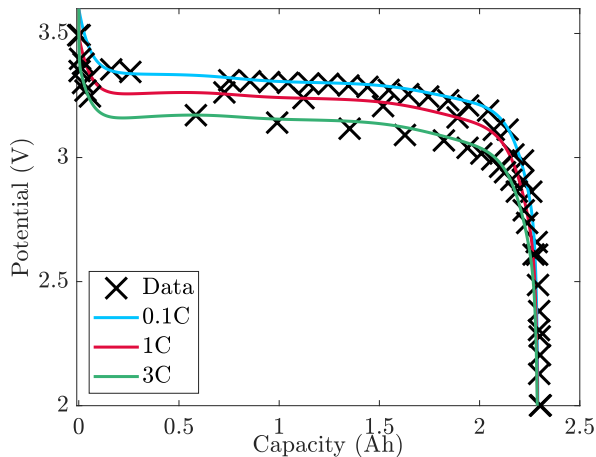


$$\frac{dy}{dt} = f(y, t), \quad y(0) = y_0$$

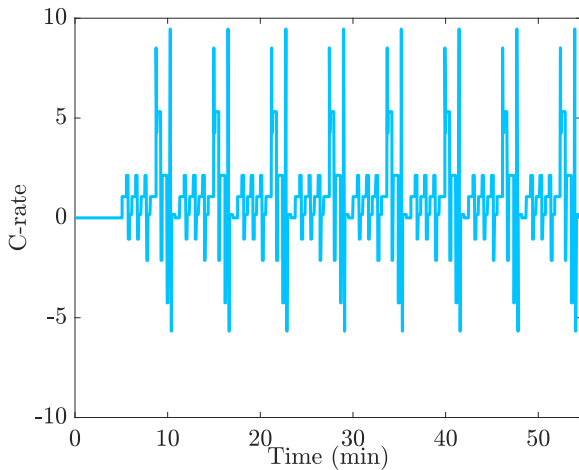
Cell Voltage-Li *et al.*



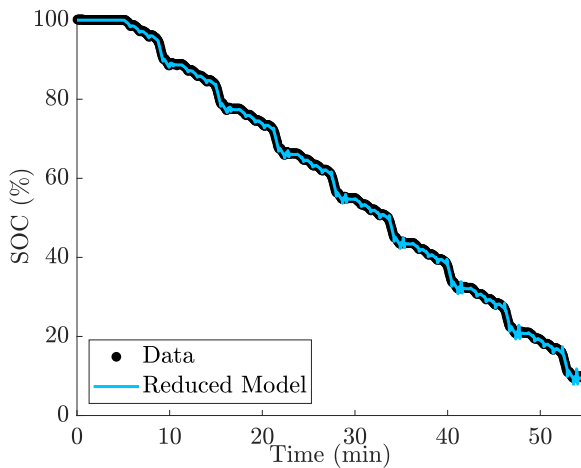
Cell Voltage-Safari and Delacourt



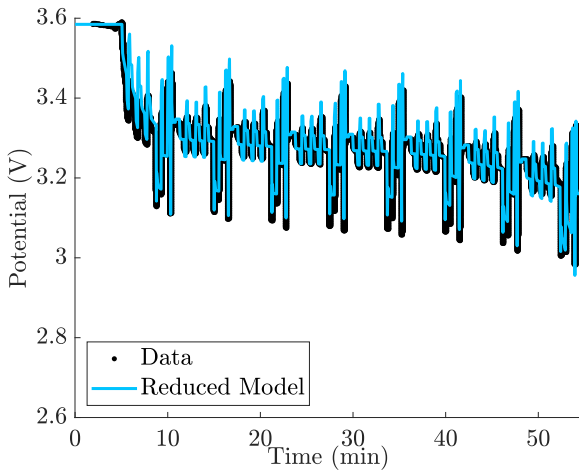
Non-Galvanostatic Discharge



Non-Galvanostatic Discharge



Non-Galvanostatic Discharge



Summary

- Mathematics can be used to extract important features from model
- Simpler and faster model derived
- Can also provide insight when model fails
 - May hint that the microscale is playing an important role

Future Work

- Add temperature
- Investigate breakdown of volume average approach

Questions?